

Lime Mud Filter (LMF) Optimization

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Mr. Tobin Alt

Vice President - Chemical Pulping Group

Kadant Black Clawson LLC

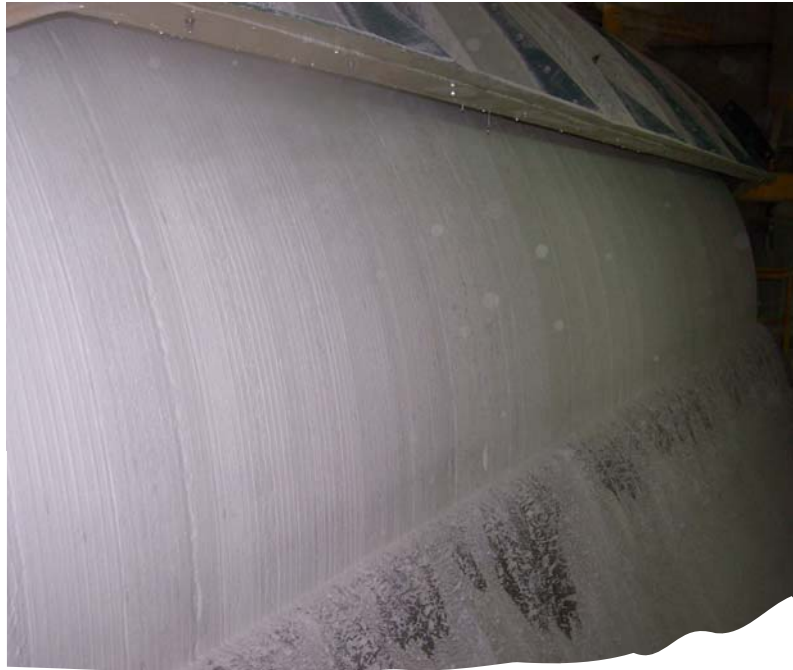
Lebanon, OH

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Presentation Agenda – What Affects LMF Solids?

- 5 Things Dictate LMF Discharge Solids & Washing Efficiency
 - 4 – Process Parameters
 - 1 – Mechanical Configuration

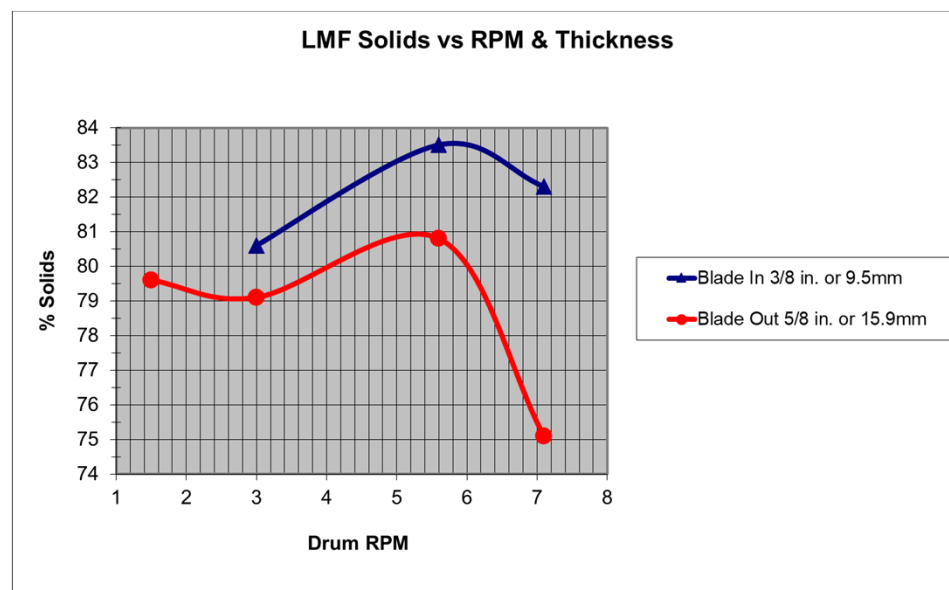
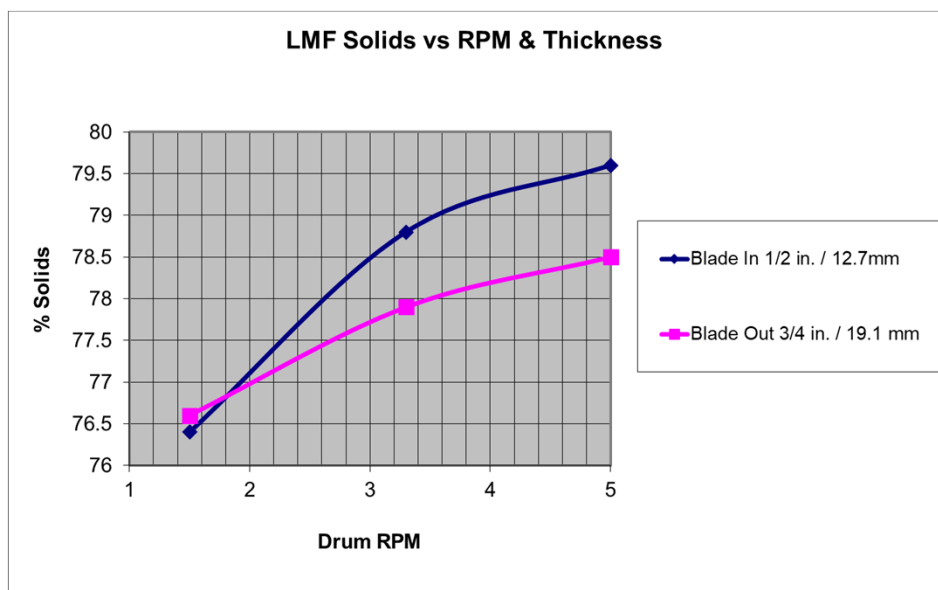
- 1. Overall Cake Thickness
- 2. Feed Slurry Density and Temperature
- 3. Shower Bar Configuration – Temperature & Location of Bars
- 4. Permeability of Lime Mud Precoat – Particle Size & Reprecoater Operation
- 5. Vacuum and Distribution Under Grids
 - 1. Internal Drum Piping Configuration & Grid Design



Ideal Appearance of Lime
Mud Filter Discharge Solids
& Cake Renewal

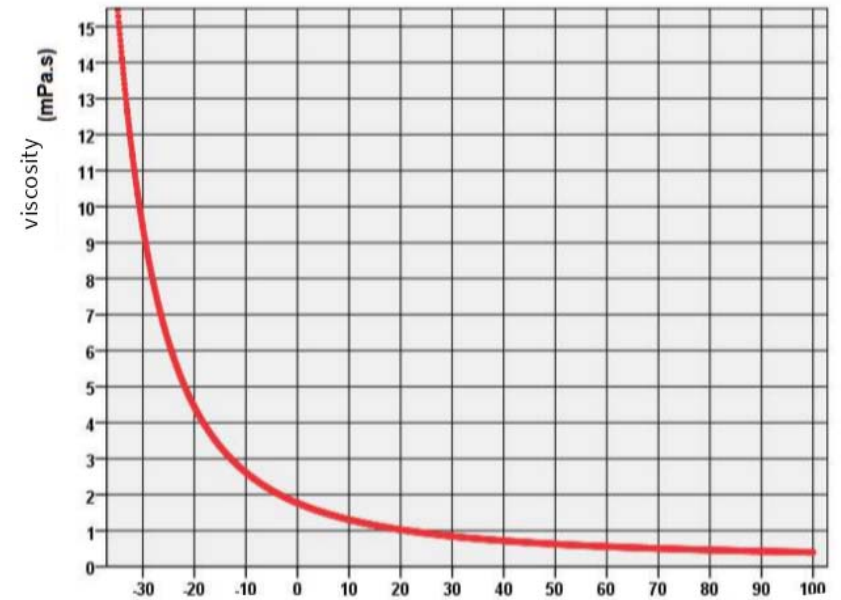
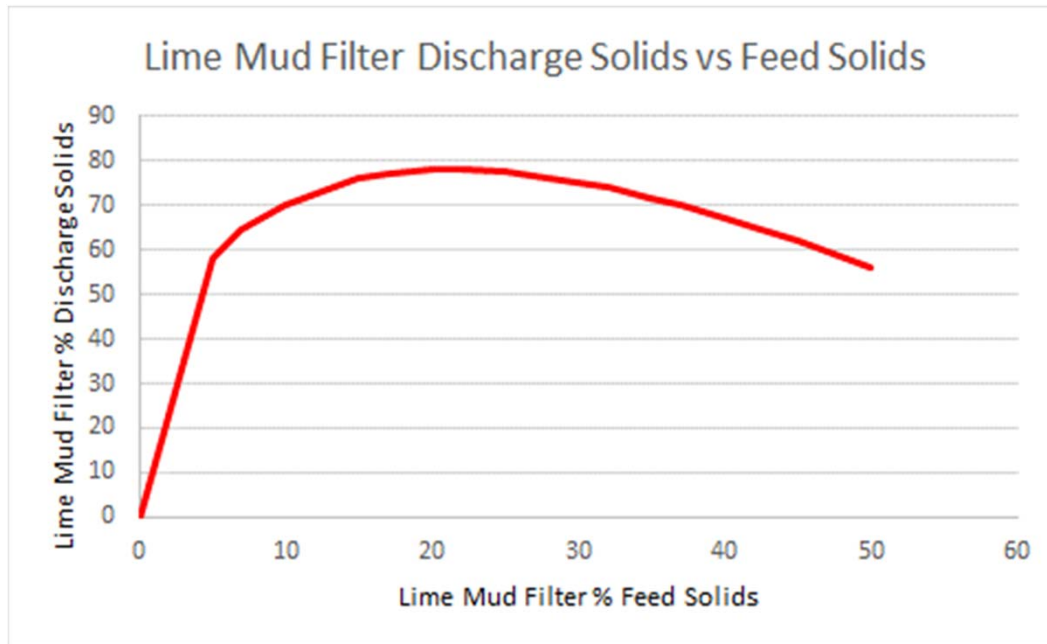
1 of 4 Four Drum Filter Process Parameters – Cake Thickness


- Overall Cake Thickness
 - Scraper Setting – 3/8" from High Point is Best in Class
 - Drum RPM – 3-4 Revolutions per Minute
 - Drum Loading < 0.75 lb Lime Mud per Square Foot of Drum Area
 - Drum Roundness – Total Indicated Runout (TIR) as Manufacture < 3/16 inch



2 of 4 Drum Process Parameters – Density/Temperature

- Feed Slurry Density and Temperature
 - Density ~ 25% Solids
 - Temperature 140°F to 160°F (60°C to 71°C)





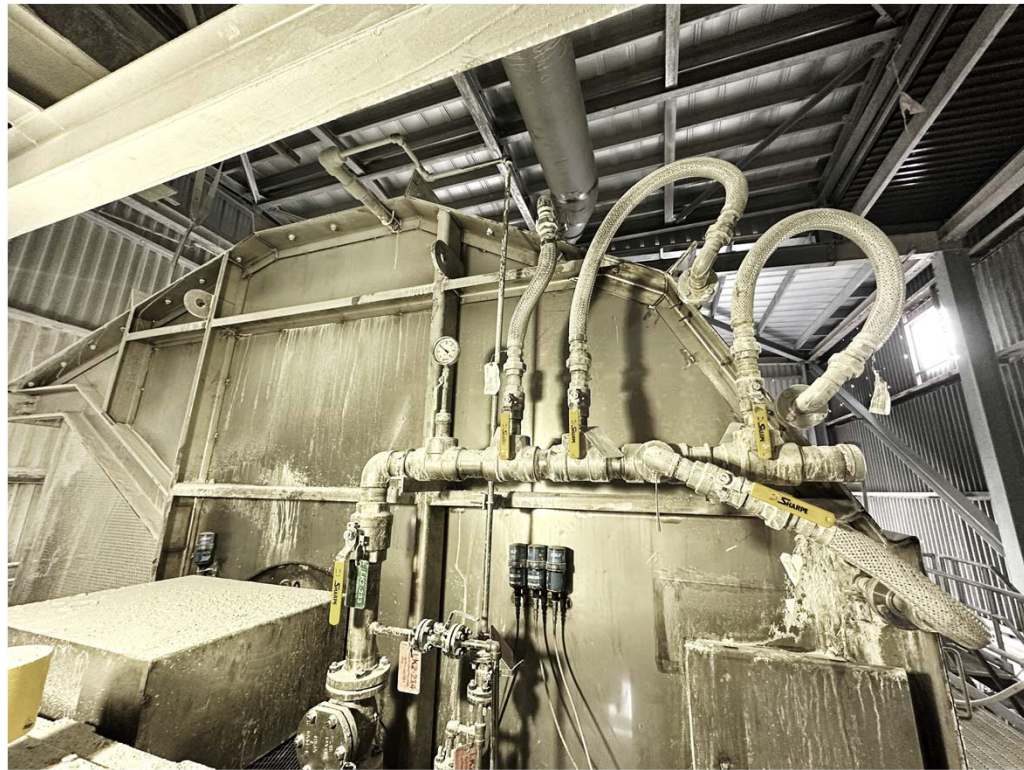
LMF Feed Slurry % Solids & Impact
40% Solids Feed & 25% Solids Feed

Blow-Off Lime Mud Filter – No Precoat
Issues: Low Solids 50-58%
Benefit: No Precoat to Blind



3 of 4 Drum Process Parameters – Cake Wash Spray Bars

Location (Internal Piping) & Temperature 160°F to 190°F (71°C to 88°C)



4 of 4 Drum Process Parameters – Particle Size Can Be Measured Via Settling Test



0m/1000ml



6.7m/910ml



38.7m/490ml



60m/280ml



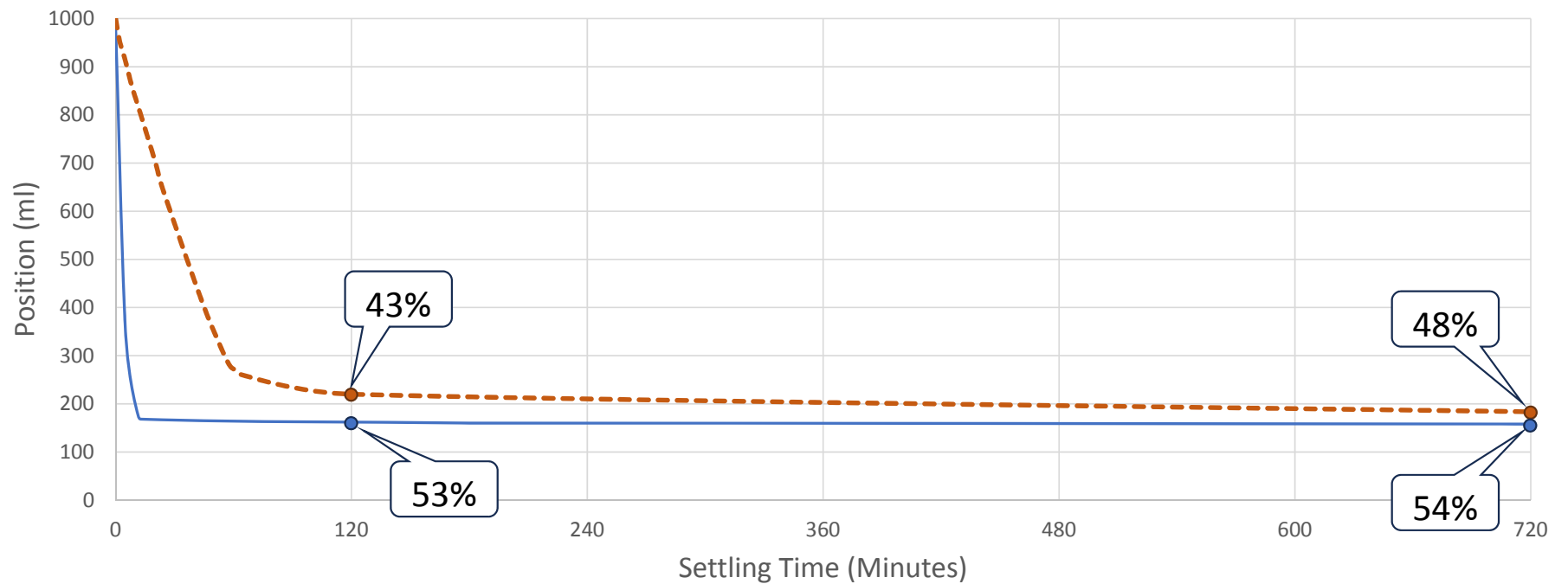
66m/260ml



180m/180ml

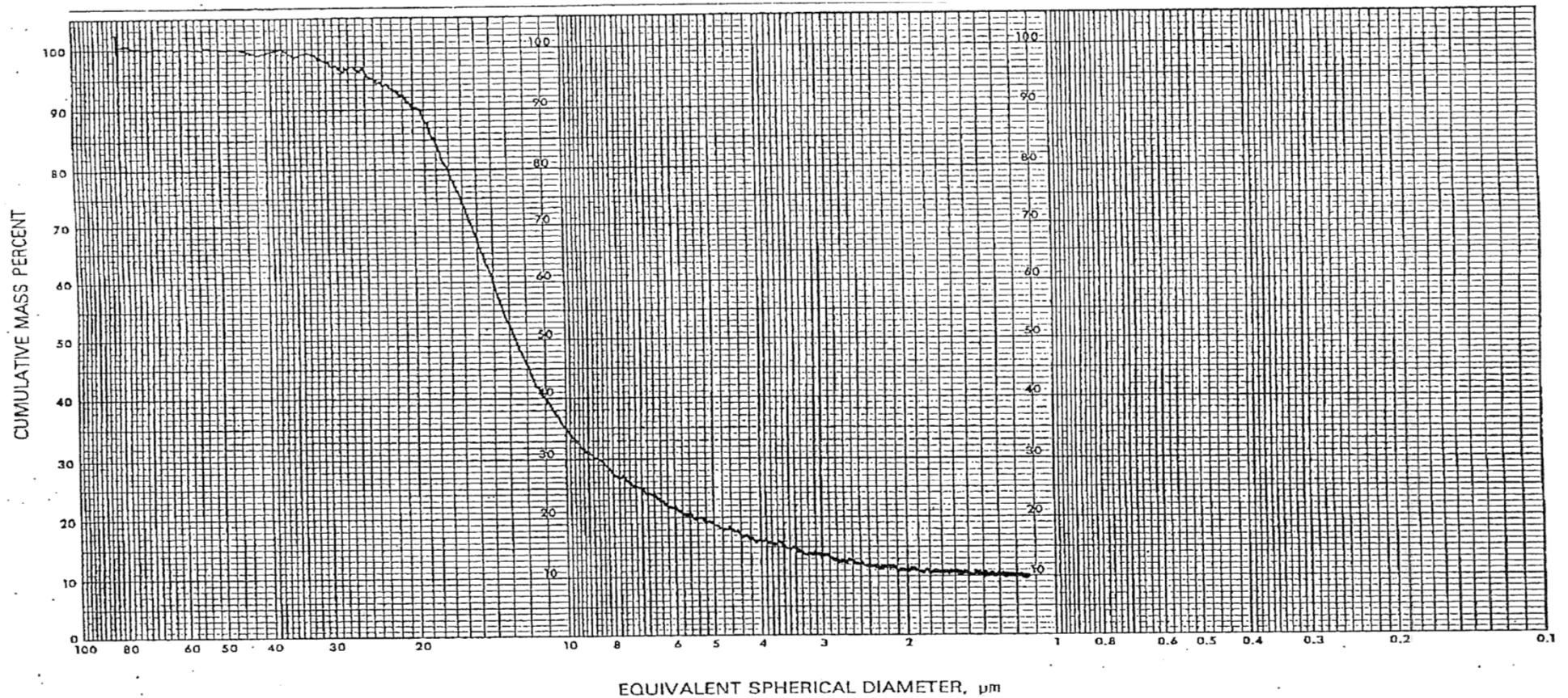
Particle Size Distribution – Measured by Settling Test

Causticized White Liquor - Both Settling & Compaction Zone



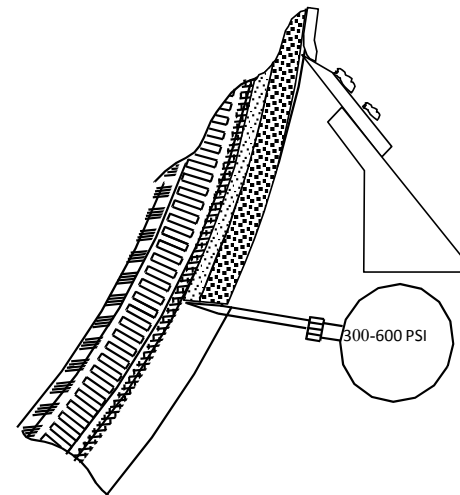
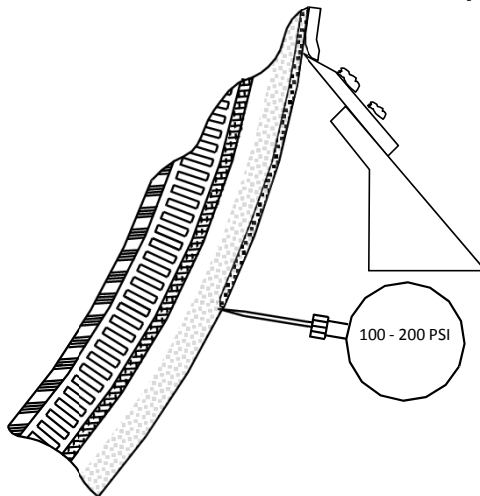
Particle Size Distribution – Process & Mechanical

Small – Over-liming, Over-Agitation, Temperature, ETC



Three (3) – Levels of Precoat Blinding

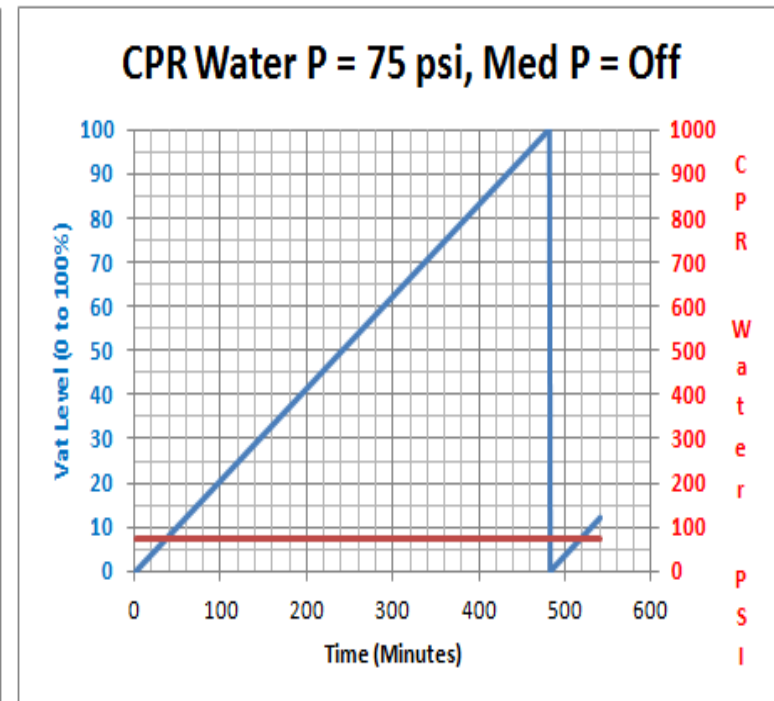
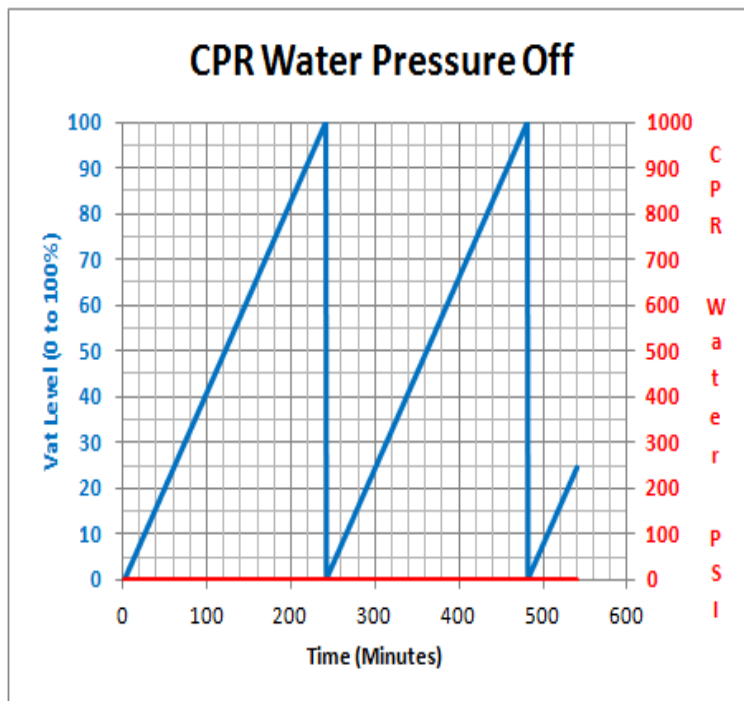
1) Outer Precoat, 2) Inner Precoat, & 3) Face Wire



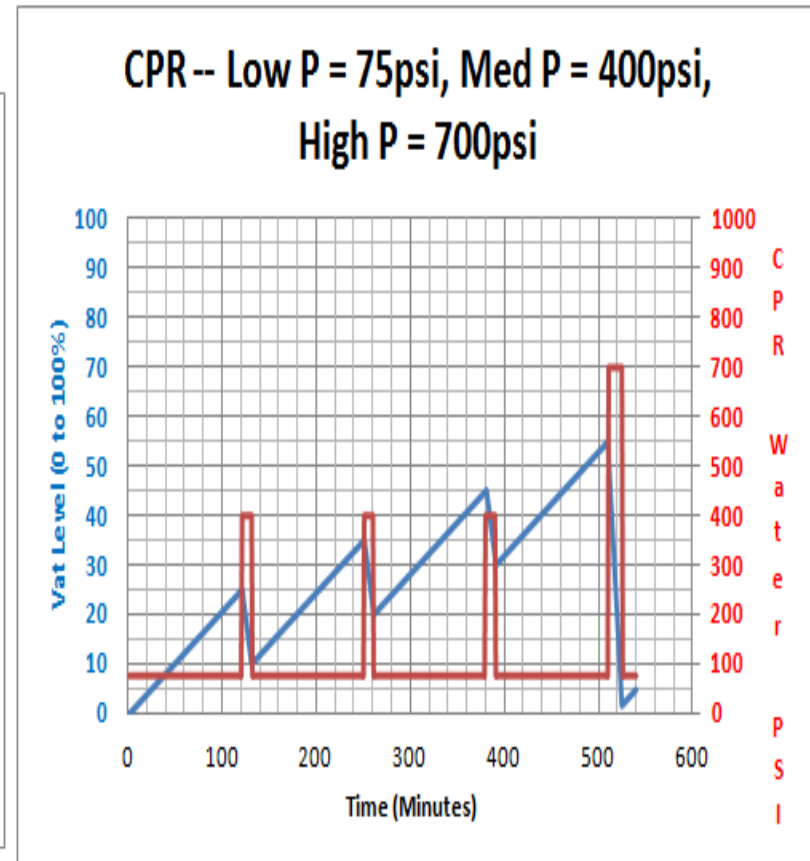
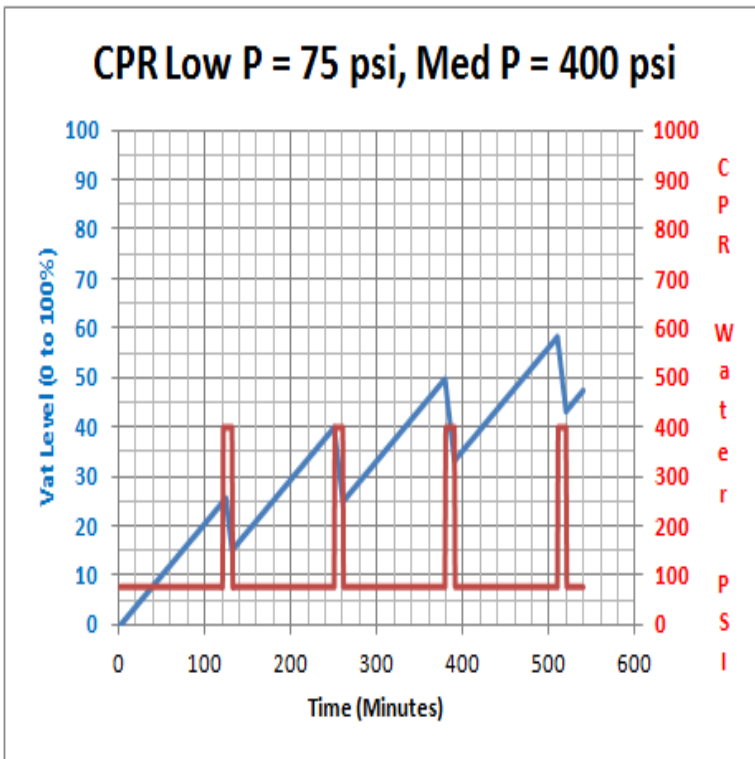
- Outer Precoat – Nozzle Penetrate $1/8 - 1/4'' = 50$ to 300 psi
- Inner Precoat – Nozzle Penetrate to Face wire = $1/2 - 3/4'' = 300$ to 1000 psi
- Face Wire – Nozzle Penetrate to Face Wire w/Force = 700 to 1000 psi

Reprecoater Optimization

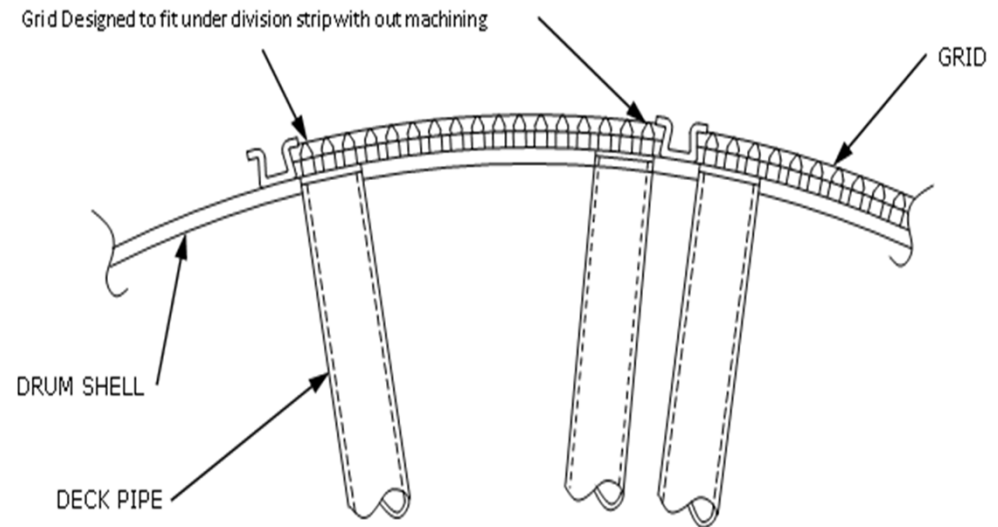
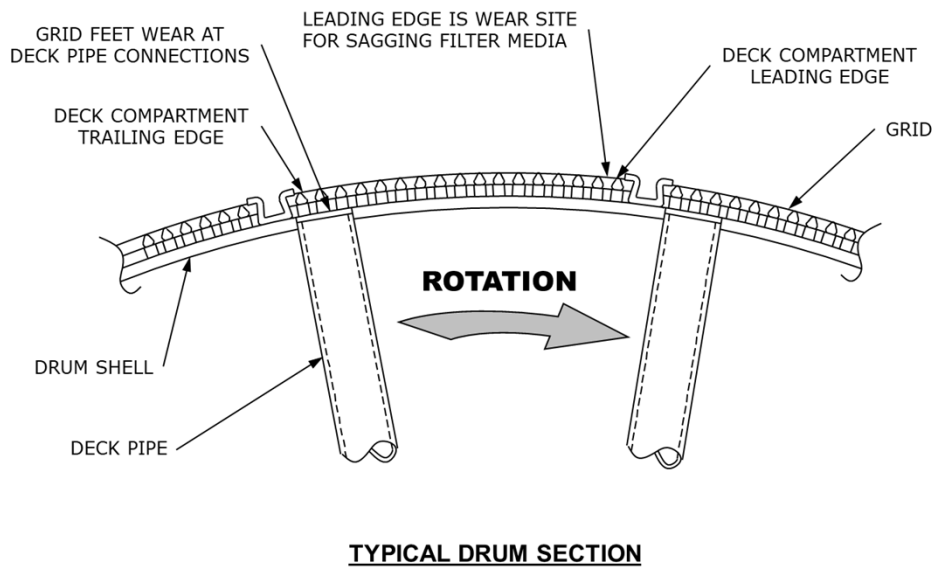
1. Use MINIMUM water pressure to maintain precoat permeability
 1. Vat level is the primary indicator
 2. Excessive water pressure: 1) Wears the face wire out, and 2) Lowers Solids



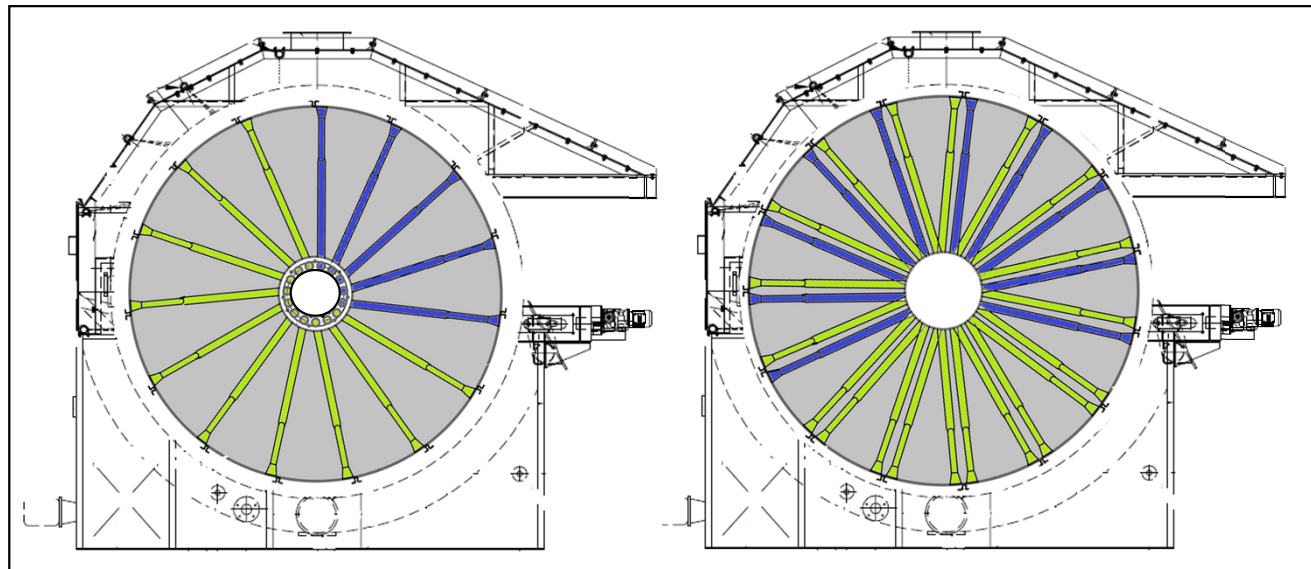
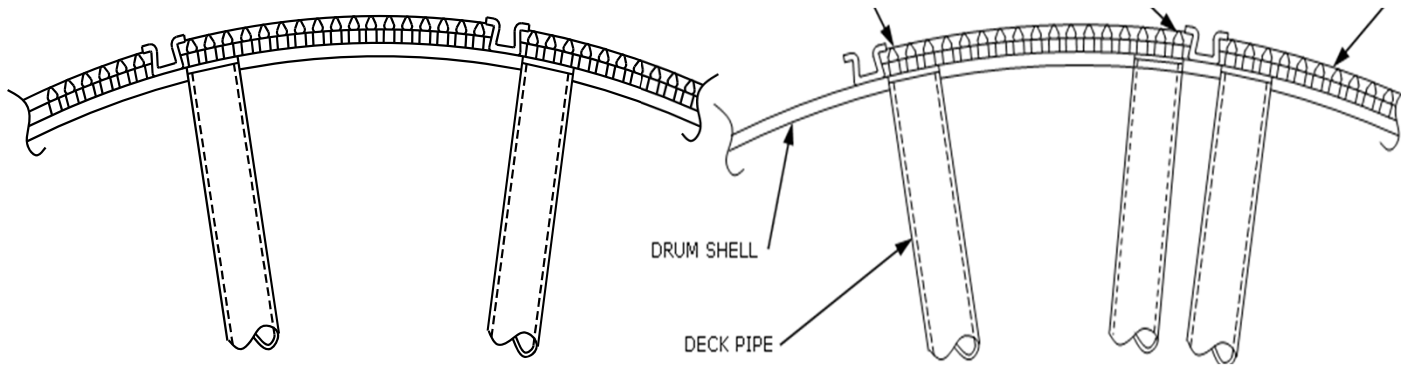
Base Pressure Increase = Slower Vat Level Increase
 Medium Pressure Increase = Lowers Base Vat Level



1 of 1 Mechanical Design Parameters Vacuum Distribution Under Grids Ideal = Pressure Same Everywhere in Section



Leading and Trailing Pipes – Dictates Solids & Washing Efficiency

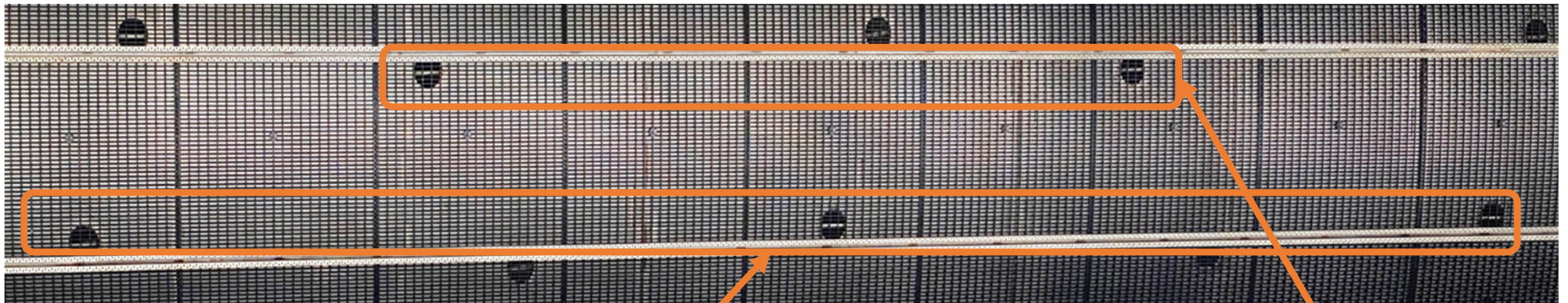


Drum – View is Rising Side

- 2 Leading Pipes
- 2 Trailing Pipes

Vacuum Distribution = Many Inlets & Tall Grids

3 Trailing and 2 Leading Pipes



3 Trailing Pipes

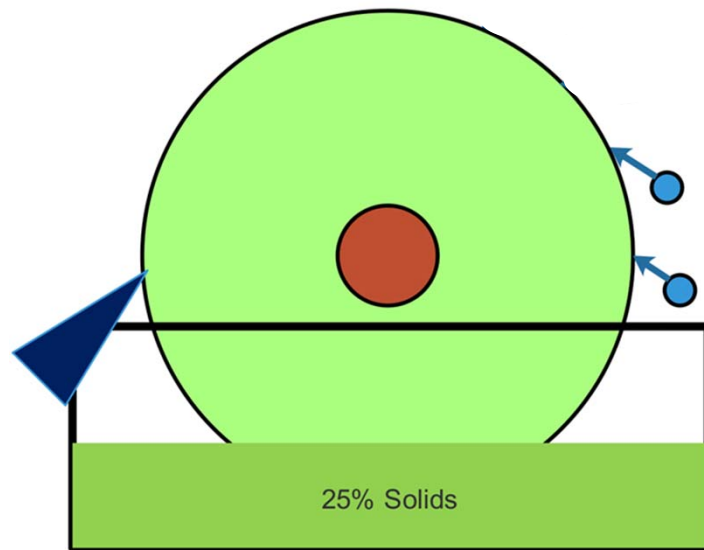
2 Leading Pipes

Poor Vacuum Distribution – Few Inlets & Short Grid Legs

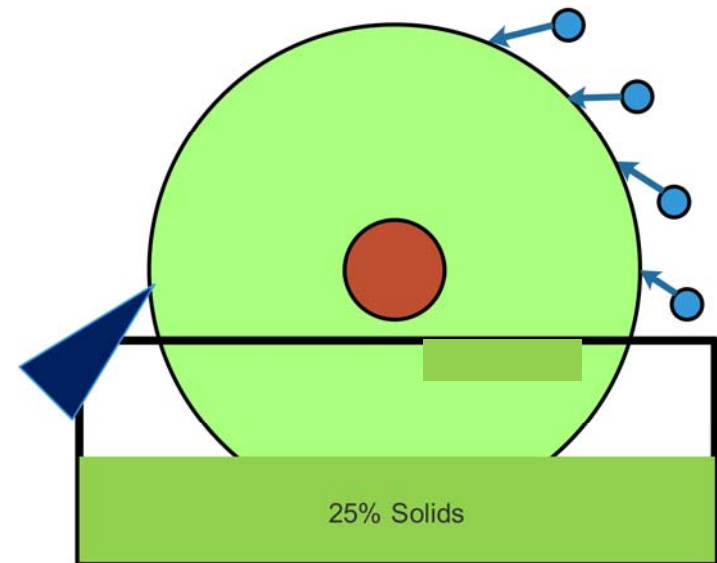


Leading & Trailing Pipes – Shower Bars 9 to 12 O-Clock No Leading Pipe Inlets = Shower Bars Can ONLY Be Low

**Internal Drum Piping Trailing Only
Shower Bars Must Be Low on Drum**



**Internal Drum Piping Leading+Trailing
Shower Bars Can Go to 12 O'Clock**



Presentation End

Questions?